



## In-Class Exercises n° 02

### (Distillation – Flash Distillation)

#### Exercise 01: Flash Equilibrium of a Binary n-Heptane/n-Octane Mixture

A liquid mixture of **100 mol** containing **50 mol%** n-heptane and **50 mol%** n-octane at **30°C** is to be continuously flash vaporized at 1 std atm to vaporize **60 mol%** of the feed. What will be the composition of the vapor and liquid for an equilibrium stage?

|                                           |     |       |       |       |        |   |
|-------------------------------------------|-----|-------|-------|-------|--------|---|
| Mole fractions of n-heptane in liquid $x$ | 1.0 | 0.655 | 0.487 | 0.312 | 0.1571 | 0 |
| Mole fractions of n-heptane in vapor $y$  | 1.0 | 0.810 | 0.674 | 0.492 | 0.297  | 0 |

#### Exercise 02:

Using mass balances for a single-stage flash distillation process, give the general operating line equation, where this equation relates the compositions of the two phases leaving the flash drum.

- 1.1) Define the **fraction vaporized**  $f = \frac{V}{F}$  and, using the total mass balance, derive the expression of the ratio  $\frac{L}{V}$  in terms of  $f$ .

Show that:

$$\frac{L}{V} = \frac{1-f}{f}$$

- 1.2) Determine  $\frac{F}{V}$  in terms of  $f$ .

- 1.3) Substitute these two expressions into the general operating line equation and simplify to obtain

$$y = -\left(\frac{1-f}{f}\right)x + \frac{z}{f}$$

- 1.4) Interpret physically the **slope** and **intercept** of this linear relationship between  $y$  and  $x$ .

- 2.1) Define the **fraction of liquid remaining**  $q = \frac{L}{F}$ .

- 2.2) Using again the total mass balance, derive the expression of  $\frac{L}{V}$  and  $\frac{F}{V}$  in terms of  $q$ .

Show that:

$$\frac{L}{V} = \frac{q}{1-q} \quad \text{and} \quad \frac{F}{V} = \frac{1}{1-q}$$

- 2.3) Substitute these results into the general operating line equation and simplify to obtain:

$$y = -\left(\frac{q}{1-q}\right)x + \frac{1}{1-q}z$$



### **Exercise 03: Multi-component Flash**

Calculate the **vapor ratio**,  $\psi$ , and the vapor and liquid stream compositions for a multi-component flash operation. The feed mole fractions and phase equilibrium constants (at the flash temperature and pressure) are provided in Table 1. Given that the feed flow is **1 250 lbmol/h**, what are the liquid and vapor molar flow rates?

**Table 1** – Multi-component Flash Data for Practical Example

| Component | Mole fraction ( $z_i$ ) | Equilibrium ratio ( $K_i$ ) |
|-----------|-------------------------|-----------------------------|
| 1         | 0.28                    | 2.93                        |
| 2         | 0.24                    | 1.55                        |
| 3         | 0.24                    | 0.87                        |
| 4         | 0.08                    | 0.49                        |
| 5         | 0.16                    | 0.138                       |