

People's Democratic Republic Of Algeria
MINISTRY OF HIGHER EDUCATION AND SCIENTIFIC RESEARCH
Abdelhafid Boussouf University Center - Mila
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Introduction to Transport Phenomena

Course Notes

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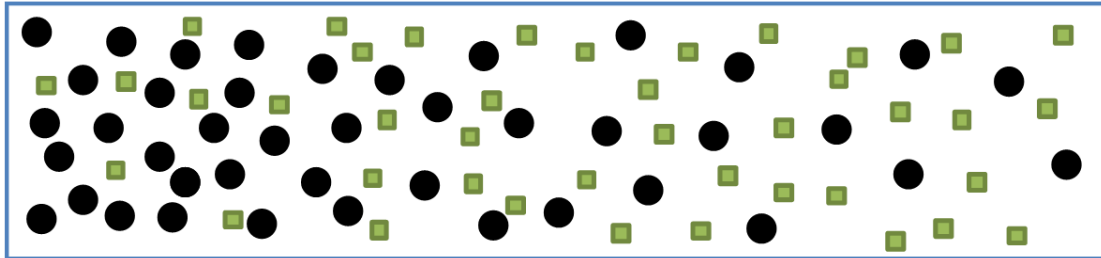
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Chapter 3

Mass Transfer

REMINDER:**1. Mass Transfer:**

Mass transfer is the net movement of a component in a mixture from one location to another location where the component exists at a **different concentration**.

**2. Modes of mass transfer:**

- Diffusion:

Transfer of molecules by **random motion** from high concentration to low concentration.

- Convection:

The use of mechanical force or action to increase the rate of molecular diffusion is convection.

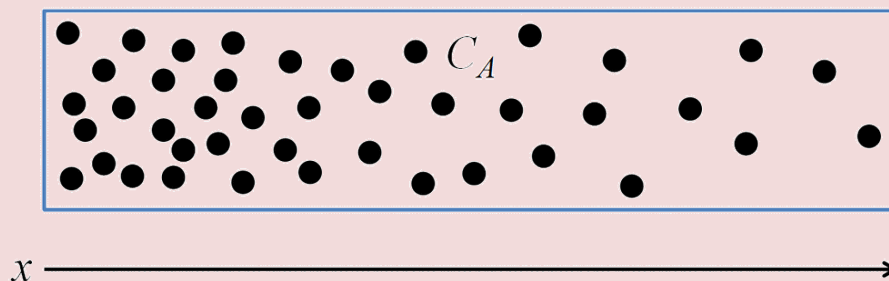
3. Concentration profiles :

A *concentration profile* is a sketch that indicates the magnitude of the concentration as a function of position $C = f(x)$. This sketch is often superimposed on a process to indicate where these changes occur.

This is analogous to a velocity profile for fluid flow.

Exercise: Concentration profile

Based on the molecular distribution below, draw the concentration profile of species A as a function of x :



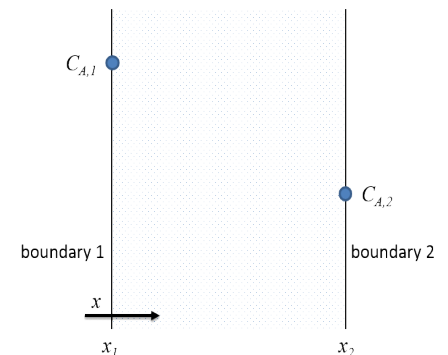
Exercise: Quick questions

1. Mass transfer occurs because of gradient in what quantity?
 - a. temperature
 - b. pressure
 - c. fluid flow
 - d. concentration
2. The two main types of mass transfer are:
 - a. diffusion and conduction
 - b. convection and diffusion
 - c. radiation and convection
 - d. conduction and radiation

1. DIFFUSION**1.1. Describing diffusion quantitatively****Exercise: Diffusion**

Suppose we have molecule A diffusing in a domain between boundary 1 and boundary 2, where $C_{A,1}$ and $C_{A,2}$ are held fixed.

What happens to C_A between boundary 1 and boundary 2 and what is the rate of diffusional mass transfer (*moles/time*) across some area A ? Note that A represents an area y by z into the figure.

**1.2. Fick's law of diffusion**

$$\dot{N}_{A,x} = -D_{AB} A \frac{dc_A}{dx}$$

For a system in which there is pure diffusion only (no convection, no reactions, constant properties), the *concentration profile* is **linear**.

Thus, Fick's law can be approximated by

$$\dot{N}_{A,x} = -D_{AB} A \left(\frac{c_{A,2} - c_{A,1}}{x_2 - x_1} \right) = -D_{AB} A \left(\frac{\Delta c_A}{\Delta x} \right)$$

Hence, the driving potential for diffusional mass transfer is: $C_{A,2} - C_{A,1}$.

In the above equations,

Variable	Definition	Typical units
$\dot{N}_{A,x}$	moles of species <i>A</i> transferred per unit time from location 1 to location 2	mol /s
D_{AB}	the 'binary diffusivity' (or diffusion coefficient) of species <i>A</i> through medium <i>B</i>	m ² /s
A	the 'face' area through which transfer occurs	m ²
$c_{A,2} - c_{A,1}$	the difference in concentration between locations 2 and 1	mol /m ³
$x_2 - x_1$	the distance between locations 2 and 1	m

Exercise: Fick's law

Why is there a minus sign in Fick's law?

Response:

The negative sign of the equation indicates that diffusion occurs in a direction opposite to that of the increasing concentration. Hence, diffusion occurs in the direction of decreasing concentration of the diffusing substance, and thus, the diffusion flux is a positive quantity.

1.3. The diffusion coefficient :

One of the big unknowns in Fick's equation above is the diffusion coefficient, D_{AB} . The diffusion coefficient (or diffusivity) is **proportionality constant** between the molar flux due to molecular diffusion and the gradient in the concentration of the species (or the driving force for diffusion).

On a theoretical basis, the *diffusion coefficient* is proportional to the mean squared displacement divided by the time:

$$D \propto \frac{\langle x^2 \rangle}{t}$$

Properties will influence the diffusion coefficient of molecule **A** in solution **B**:

molecular size of **A** and/or **B**; molecular weight of **A** and/or **B**; temperature; pressure ...etc.

Exercise:

What are some typical values of diffusion coefficients? Which coefficients will be largest?

- Gases?
- Liquids?
- Solids?

Substance A	Substance B	T, K	D_{AB} or $D_{BA}, m^2/s$	Substance A (Solute)	Substance B (Solvent)	T, K	$D_{AB}, m^2/s$	Substance A (Solute)	Substance B (Solvent)	T, K	$D_{AB}, m^2/s$
Argon, Ar	Nitrogen, N ₂	293	1.9×10^{-5}	Ammonia	Water	285	1.6×10^{-9}	Carbon dioxide	Natural rubber	298	1.1×10^{-10}
Carbon dioxide, CO ₂	Benzene	318	0.72×10^{-5}	Benzene	Water	293	1.0×10^{-9}	Nitrogen	Natural rubber	298	1.5×10^{-10}
Carbon dioxide, CO ₂	Hydrogen, H ₂	273	5.5×10^{-5}	Carbon dioxide	Water	298	2.0×10^{-9}	Oxygen	Natural rubber	298	2.1×10^{-10}
Carbon dioxide, CO ₂	Nitrogen, N ₂	293	1.6×10^{-5}	Chlorine	Water	285	1.4×10^{-9}	Helium	Pyrex	773	2.0×10^{-12}
Carbon dioxide, CO ₂	Oxygen, O ₂	273	1.4×10^{-5}	Ethanol	Water	283	0.84×10^{-9}	Helium	Pyrex	293	4.5×10^{-15}
Carbon dioxide, CO ₂	Water vapor	298	1.6×10^{-5}	Ethanol	Water	288	1.0×10^{-9}	Helium	Silicon dioxide	298	4.0×10^{-14}
Hydrogen, H ₂	Nitrogen, N ₂	273	6.8×10^{-5}	Glucose	Water	298	0.69×10^{-9}	Hydrogen	Iron	298	2.6×10^{-13}
Hydrogen, H ₂	Oxygen, O ₂	273	7.0×10^{-5}	Hydrogen	Water	298	6.3×10^{-9}	Hydrogen	Nickel	358	1.2×10^{-12}
Oxygen, O ₂	Ammonia	293	2.5×10^{-5}	Methane	Water	275	0.85×10^{-9}	Hydrogen	Nickel	438	1.0×10^{-11}
Oxygen, O ₂	Benzene	296	0.39×10^{-5}	Methane	Water	293	1.5×10^{-9}	Cadmium	Copper	293	2.7×10^{-13}
Oxygen, O ₂	Nitrogen, N ₂	273	1.8×10^{-5}	Methane	Water	333	3.6×10^{-9}	Zinc	Copper	773	4.0×10^{-18}
Oxygen, O ₂	Water vapor	298	2.5×10^{-5}	Methanol	Water	288	1.3×10^{-9}	Zinc	Copper	1273	5.0×10^{-13}
Water vapor	Argon, Ar	298	2.4×10^{-5}	Nitrogen	Water	298	2.6×10^{-9}	Antimony	Silver	293	3.5×10^{-15}
Water vapor	Helium, He	298	9.2×10^{-5}	Oxygen	Water	298	2.4×10^{-9}	Bismuth	Lead	293	1.1×10^{-20}
Water vapor	Nitrogen, N ₂	298	2.5×10^{-5}	Water	Ethanol	298	1.2×10^{-9}	Mercury	Lead	293	2.5×10^{-19}
				Water	Ethylene glycol	298	0.18×10^{-9}	Copper	Aluminum	773	4.0×10^{-14}
				Water	Methanol	298	1.8×10^{-9}	Copper	Aluminum	1273	1.0×10^{-13}
				Chloroform	Methanol	288	2.1×10^{-9}	Carbon	Iron (fcc)	773	5.0×10^{-15}
								Carbon	Iron (fcc)	1273	3.0×10^{-11}

2. MASS CONVECTION :

Mass transfer by convection involves material transport between a boundary surface (such as a solid or liquid surface) and a moving fluid or between two relatively immiscible, moving fluids.

2.1. Newton's law of cooling

To quantify the rate of mass transfer owing to convection, we can use Newton's law of cooling (which also applies to *convective heat transfer*).

Newton's law of cooling for mass transfer:

$$\dot{N}_A = h_m A (c_{A,s} - c_{A,\infty})$$

Hence, the driving potential for convective mass transfer is: $C_{A,s} - C_{A,\infty}$

In the above equations,

Variable	Definition	Typical units
$\dot{N}_{A,x}$	moles of species A transferred per unit time from the surface to the bulk fluid far from the surface	mol /s
h_m	the mass transfer coefficient	m/s
A	the area (cross section) through which transfer occurs	m ²
$c_{A,s} - c_{A,\infty}$	the difference in concentration between the surface and bulk fluid	mol /m ³